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### **RESEARCH ARTICLE**

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# Measurement of Solubility of Anthracene in Supercritical Carbon Dioxide by the Synthetic-Static Method Using *Insitu* UV-Visible Spectroscopy

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## ABSTRACT

Solubilities of anthracene in supercritical carbon dioxide in the pressure range of 8–25 MPa at 313.2 and 333.2 K were measured by the synthetic-static method, in which saturation states, i.e. equilibrium pressures, were determined using an *in-situ* UV-visible spectroscopy under static conditions. The experimental solubilities of anthracene at the present conditions were in the range of  $1 \times 10^{-6} - 2 \times 10^{-4}$  in mole fraction and the crossover pressure between the solubility at 313.2 K and that at 333.2 K was around 15 MPa. The experimental solubilities were in good agreement with the literature data obtained by the analytical methods including flow methods, recirculation methods, and spectroscopic methods with an average absolute deviation of lower than 10%. The present measurement method is very effective for the solubilities were correlated by the Chrastil equation, which is one of the semi-empirical equations. The present model gave good correlation results for the experimental data. *Keywords* - Solubility, anthracene, supercritical carbon dioxide, synthetic method, modelling

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#### I. INTRODUCTION

Supercritical fluids have been given much attention as a new type of solvent and have been applied in various industries [1, 2]. In particular, carbon dioxide has been commonly used as a solvent for many industrial applications because it is environmentally benign, nonhazardous, and inexpensive and has a low critical temperature and a moderate critical pressure [1-3].

A knowledge of solubility data of solutes in supercritical carbon dioxide is very important to the understanding and design of processes with supercritical carbon dioxide [4-12]. For example, solubility data can be used to predict the applicability of crystallization processes using supercritical carbon dioxide such as the production of fine particles [7, 8, 11, 13, 14] and thin films [15-17] by rapid expansion of supercritical solutions (RESS) [18] and the production of thin films [10, 12, 19, 20] by supercritical fluids deposition (SCFD) [21, 22]. Therefore, the solubility must be determined and modeled in order to design effective processes. In particular, the pressure and temperature dependence of solubility must be understood. This will lead to engineers to optimize the operating

conditions of unit operations such as extractors, separators, transfer lines, and crystallizers.

There have been a number of different approaches developed for measuring of solubility of solutes in supercritical carbon dioxide [4, 21-24]. These methods can be divided into two major categories depending on how the compositions of the equilibrium phases are determined (analytically or not) and whether the mixture to be investigated has been prepared (synthesized) with precisely known composition or not: analytical methods and synthetic methods [4, 23-26]. The simplest, most straightforward and most commonly used methods of measuring solubility will be the analytical-flow method. In the method, the extractor is filled with and supercritical solutes, carbon dioxide continuously flows through the extractor. The solutes and solvent are then separated by density difference, and the concentration of the sampled solutes is analyzed by various techniques including chromatographic, spectroscopic, gravimetric, and other techniques. In the method, it is important to ensure that the solutes and solvent, i.e., supercritical carbon dioxide, achieve equilibrium while the solvent is flowing through the extractor. Therefore,

it is difficult to measure solubility in supercritical carbon dioxide by the method when the solutes loading in the extractor is very small, e.g., when the solutes cost is high, and when the sampling amount of solutes is small, e.g., when the solubility of the solutes is small, because accurately measuring the concentration of solutes is very difficult with techniques such as chromatography and gravimetry. The spectroscopic technique has been one of powerful tools to measure solubility of solutes in supercritical carbon dioxide. It requires no sampling of the solutes, which overcomes many drawbacks of the analytical-flow method. Various studies have been reported in the literature for the past years, either using ultraviolet (UV)-visible spectroscopy [27-29], infrared (IR) spectroscopy [30-32], nearinfrared (NIR) spectroscopy [33, 34], Raman spectroscopy [35], and fluorescence spectroscopy [36]. These spectroscopic measurement techniques need a calibration curve or molar absorptivity prepared with supercritical carbon dioxide or several organic solvents. However, calibration curves and molar absorption coefficients prepared using supercritical carbon dioxide and various organic solvents are not applicable because they differ from the actual ones due to the density dependence of carbon dioxide [37] and differences in absorption peaks caused by solvatochromism when the solution has absorption in the visible region [38].

Ngo et al. [39] proposed a new synthetic method to measure the solubility of solutes in supercritical carbon dioxide, in which saturation states, i.e., equilibrium of the mixture, were determined using an in-situ UV-visible, IR, or fluorescence spectroscopy under static conditions. The method is the static method, in which the vessel is charged with a known amount of solutes and it was pressurized with carbon dioxide and stirred constantly. Equilibrium of the mixture was observed in-situ by periodically taking UV, IR, or fluorescence spectra of the solution. The pressure was raised stepwise until no further significant increase in the peak absorbance was observed. This meant that all solids had been dissolved in the fluid phase. The method is able to obtain solubility data without performing any calibration prior to the experiments or making any assumptions on the constancy of the molar absorptivity. They proposed that IR is suitable for measuring the solubility higher than  $10^{-5}$  in mole fraction, UV is appropriate for solubility higher than  $10^{-6}$  in mole fraction, and fluorescence is suitable for measuring the solubility of about  $10^{-7}$  in mole fraction.

In the present work, solubilities of anthracene in supercritical carbon dioxide in the pressure range of 8–25 MPa and at the temperatures 313.2 and 333.2 K were measured by the synthetic-

static method using an *in-situ* UV-visible spectroscopy proposed by Ngo *et al.* [39]. Anthracene was used as a model acene because it is a promising material for fabricating several organic semiconductors [40–46] and blue OLEDs [47, 48]. Because the experimental determination of solubility of solutes in supercritical carbon dioxide is difficult, costly, and time consuming, it is advantageous to extend and complement the experimental data with some model. Therefore, the solubilities obtained were correlated by the Chrastil equation [49], a semi-empirical equation that has been reported to have the highest correlation accuracy for solutes solubility in supercritical carbon dioxide [50].

#### **II. EXPERIMENTAL**

## 2.1 Materials

Anthracene (supplied by Acros Organics of Themo Fisher Scientific Inc.; the purity is > 99%; molecular weight is 178.23) was used as a solute. Fig. 1 shows the chemical structure of anthracene. High-purity  $CO_2$  (its purity is > 99.99%, supplied by Showa Denko Gas Products Co., Ltd.) was used as a solvent and was supplied through a dryer, in which 5A molecular sieve particles were packed to remove impurities such as water.

### 2.2 Apparatus and Procedures

A static equilibrium apparatus was used in this work. A schematic diagram of the apparatus used in this work is shown in Fig. 2.

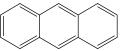
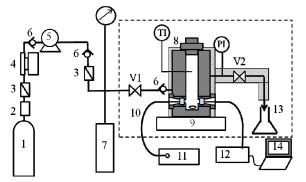


Fig. 1 Chemical structure of anthracene.



<sup>Fig. 2 Schematic diagram of the experimental setup: 1. CO<sub>2</sub> gas cylinder, 2. dryer, 3. filter, 4. cooling unit, 5. screw-type hand-pump, 6. stopper, 7. CO<sub>2</sub> reservoir, 8. high-pressure optical cell, 9. magnetic stirrer, 10. optical fibers, 11. UV-vis light source, 12. UV-vis spectrophotometer, 13. Glass trap, 14. personal computer, \_\_\_\_\_ heating jackets, \_\_\_\_\_\_ dark booth.</sup> 

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Known amounts of a solute were introduced into the high-pressure optical cell, having a direct path with two sapphire windows (8) (Taiatsu Techno Co.), in solid form (> 0.10 mg) or in toluene solution (< 0.01 mg). When the solute was added in the solution form, the toluene was evaporated in the cell at 313.2 K for 12 h. After loading, the cell was heated to a desired temperature by heating jackets. The pressurized carbon dioxide was then introduced into the cell to a desired pressure, and stirred constantly. The supercritical carbon dioxide was in contact with solid solute at the pressure and temperature. Equilibrium of the mixture was observed in-situ by periodically taking UV spectra of the solution (12) (Hamamatsu Photonics K.K. PMA-12, C10544-01). The spectral change of anthracene with increasing pressure of supercritical carbon dioxide is shown in Fig. 3. The pressure of carbon dioxide was increased up until there was no further increase in the peak absorbance. The absorbance was obtained using the average absorbance in the whole of peak wavelength to reduce a significant spectral shift, as shown in the following equation (1):

$$A_{\rm ave} = \left(\int_{a}^{b} A(\lambda) \mathrm{d}\lambda\right) / (b-a) \tag{1}$$

 $A_{\rm ave}$  is the average absorbance calculated by integration of the absorbance in the wavelength range from a to b and  $A(\lambda)$  is the absorbance at the wavelength  $\lambda$ . In a preliminary examination, we determined the values of a and b as 310 nm and 385 nm, respectively. The average absorbance was plotted versus the pressure as shown in Fig. 4. As the pressure increased, there was a large increase in solubility of the solute in supercritical carbon dioxide. Once all the solute in the cell dissolved, there was an abrupt change in the slope and the absorbance became almost constant. The pressure at saturation was then determined from the intersection of the two linear regions on the graph as shown in Fig. 4. For example, we can determine the saturation pressure is 9.08 MPa. Solubility can be calculated by the mass of solute in the cell, the fluid density at saturation, and the cell volume. The density of carbon dioxide was calculated from the Span-Wagner equation [51]. The solubility in mole fraction of the solute in supercritical carbon dioxide,  $v_2$  was calculated by the following equation (2):

$$y_{2} = \frac{w/M_{s}}{(V \times \rho / M_{CO2}) + w/M_{s}}$$
(2)

where w is the mass of the solute,  $M_{\rm S}$  and  $M_{\rm CO2}$  are the molar masses of the solute and carbon dioxide, respectively. V is the volume of the high-pressure optical cell, and  $\rho$  is the density of carbon dioxide at the experimental condition.

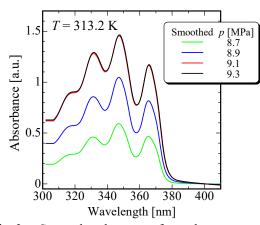
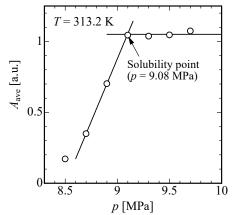
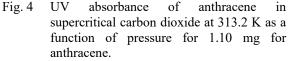


Fig. 3 Spectral change of anthracene with increasing pressure of supercritical carbon dioxide at 313.2 K.





# III. RESULTS AND DISCUSSION 3.1 Experimental results

The experimental solubilities of anthracene in supercritical carbon dioxide at 313.2 and 333.2 K were shown in Fig. 5 and Table 1, and Fig. 6 and Table 2, respectively. As shown in Figs. 5 and 6, The experimental solubilities of anthracene at the present conditions were in the range from  $1 \times 10^{-6}$  to  $2 \times 10^{-4}$  in mole fraction and the crossover pressure between the solubility at 313.2 K and that at 333.2 K was around 15 MPa. The experimental solubilities were in good agreement with the literature data obtained by the analytical methods including the spectroscopic method [39], flow methods [54, 56, 58], and recirculation methods [53, 55] with an average absolute deviation of lower than 10%. The self-consistency of the measured solubility was evaluated using the following equation proposed by Méndez-Santiago and Teja [59]:

$$T\ln E = T\ln(y_2 p / p_2^{\text{sat}}) = A + B\rho$$
(3)

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where *T* is the equilibrium temperature,  $\rho$  is the density of carbon dioxide that was calculated by the Span-Wagner equation. *A* and *B* are the constants: *A* = 834.7 and *B* = 0.1645, and *E* is the enhancement factor. *p* is the equilibrium pressure and  $p_2^{\text{sat}}$  is the saturated vapor pressure of anthracene which was evaluated by the Antoine equation [60]. As shown in Fig. 7, the solubility data of anthracene at the present conditions collapsed to a straight line, when plotted as *T* ln *E* vs the density of carbon dioxide, so that the present data would be internally consistent. The present measurement method is very effective for the solubility measurement of organic compounds such as anthracene with very low solubility in supercritical carbon dioxide.

#### **3.2** Correlation

The solubilities obtained were correlated by the following Chrastil equation [49]:

$$c = d^k \exp(a/T + b) \tag{4}$$

where c is the solute concentration; solubility, in supercritical carbon dioxide in kg  $\cdot$  m<sup>-3</sup>, d is the density of carbon dioxide in kg  $\cdot$  m<sup>-3</sup> which was calculated by the Span-Wagner equation, T is an absolute temperature in K. The parameters, a, b and k are Chrastil parameters those were determined to give a good representation of the experimental solubility. The parameters were thus determined as a = -5908 K<sup>-1</sup>, b = -17.55 and k = 5.2060. The calculated solubilities of anthracene in supercritical carbon dioxide are shown in Fig. 8. The present model gave good correlation results for all of the experimental solubilities of anthracene in supercritical carbon dioxide.

#### **IV. CONCLUSION**

The experimental solubilities of anthracene at the present conditions were in the range of  $1 \times 10^{-6}$ to  $2 \times 10^{-4}$  in mole fraction and those were in good agreement with the literature data with an average absolute deviation of lower than 10%. The present technique, i.e., synthetic-static method using *in-situ* UV spectroscopy, enables high-precision solubility measurement of organic compounds with low solubility using only a small amount of solutes without using a calibration curve or molar absorptivity. The solubilities were correlated by the Chrastil equation and the present models gave good correlation results for the experimental data.

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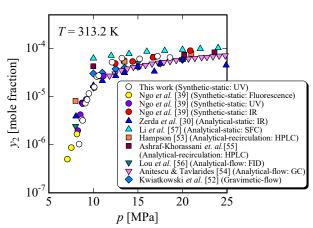
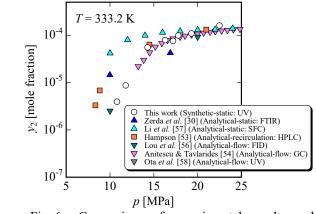


Fig. 5. Comparison of experimental results and literature data of solubility of anthracene in supercritical carbon dioxide at 313.2 K.



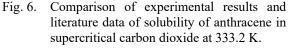


Table 1Experimental solubility data of anthracene<br/>in supercritical carbon dioxide at 313.2 K.

<i>T</i> [K]	p [MPa]	<i>y</i> <sub>2</sub> [mole fraction]
313.2	8.35	$1.02 \times 10^{-6}$
	8.67	3.39×10 <sup>-6</sup>
	8.77	3.18×10 <sup>-6</sup>
	9.08	7.27×10 <sup>-6</sup>
	9.25	$8.64 \times 10^{-6}$
	9.49	$1.15 \times 10^{-5}$
	10.05	$1.53 \times 10^{-5}$
	10.13	$1.57 \times 10^{-5}$
	10.42	$2.60 \times 10^{-5}$
	10.57	$2.72 \times 10^{-5}$
	12.06	$5.17 \times 10^{-5}$
	13.19	6.27×10 <sup>-5</sup>
	15.21	$6.05 \times 10^{-5}$
	17.21	$6.88 \times 10^{-5}$
	18.61	$6.47 \times 10^{-5}$
	21.19	$7.08 \times 10^{-5}$
	24.25	$8.79 \times 10^{-5}$

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<i>T</i> [K]	p [MPa]	$y_2$ [mole fraction]
333.2	10.76 11.85 14.33 16.25 17.17 17.83 19.26 22.46	$\begin{array}{c} 3.93 \times 10^{-6} \\ 8.70 \times 10^{-6} \\ 5.50 \times 10^{-5} \\ 7.87 \times 10^{-5} \\ 7.59 \times 10^{-5} \\ 9.87 \times 10^{-5} \\ 1.09 \times 10^{-4} \\ 1.60 \times 10^{-4} \end{array}$

Table 2Experimental solubility data of anthracene<br/>in supercritical carbon dioxide at 333.2 K.

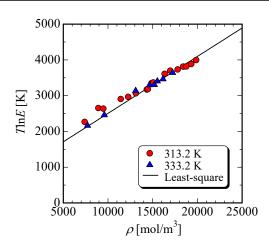


Fig. 7. Self-consistency of the experimental solubility data of anthracene in supercritical carbon dioxide.

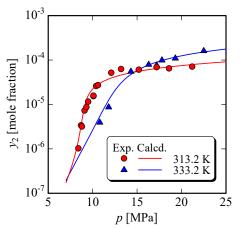


Fig. 8. Experimental and calculated solubility of anthracene in supercritical carbon dioxide.

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