

A Simple Method For Treatment Of Waste Water Containing Cu(II), Pb(II), Mn(II) And Co(II) Ions Using Adsorption On Dried Leaves

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ABSTRACT:

A new simple method for treatment of waste water effluent containing Cu(II), Pb(II), Mn(II), Co(II) was developed using *Myrtus communis* as a low-cost natural adsorbent. Batch experiments were conducted to determine the effects of varying; adsorbent weight, pH, contact time, metal ion concentration and temperature of adsorption. The adsorption of Pb (II) was found to be maximum (98.8%) at pH4, temperature of 25°C, metal ion concentration 50 ppm and contact time 90 min. Adsorption capacity of Cu (II), Mn(II), and Co(II) were found maximum (92.4%, 84.1% and 79.7%) respectively at optimum conditions. The order of removal efficiency of these metals was found Pb > Cu > Mn > Co. Freundlich isotherm was found to be suitable for the adsorption of Cu(II), Pb(II), Mn(II), Co(II). Adsorption kinetics data were found pseudo-first and pseudo-second order. The results indicate that the second-order model best describes adsorption kinetic data. Functional groups (O-H, C-O and C-N) identification were given using FTIR spectrophotometry.

Keywords: *Myrtus communis*; heavy metals; adsorption; isotherm models

INTRODUCTION

The toxicity of heavy metals in the environment is still a major concern of human life; because they accumulate in living tissues throughout the food chain which has humans at its top. The danger of these heavy metals is due to poisoning, cancer, and brain damage [1]. Therefore treatment of water and waste water containing heavy metal is very demanding. Such methods of treatment include precipitation [2], flotation [3], biosorption [4–6], electrolytic recovery, membrane separation [7], removal by adsorption on minerals [8,9] and activated carbon adsorption [10,11]. Despite these wide methods, they have disadvantages, which include incomplete metal removal requirements and expensive equipment. Recently many researchers in the world wide investigated low-cost adsorbents with high metal binding capacities. Agricultural by-products have been widely used for treatment of water containing heavy metal. These agricultural

materials include; peat, wood, pine bark, banana pith, soybean and cotton seed hulls, peanut shells, hazelnut shell, rice husk, saw dust, wool, orange peel, compost and leaves [12]. The present work is attempted to investigate the possibility of the utilization of one kind of tree leaves: *myrtus-communis* (MC) for removal of Cu(II), Pb(II), Mn(II), Co(II) from waste water. Optimization variables include; contact time, pH, temperature, particle size, and initial ion concentration. The Freundlich, Langmuir and Temkin adsorption isotherms were used to investigate the adsorption process. Kinetic study was also carried out to evaluate the order of adsorption.

Experimental:

Chemical, reagent procedure and instruments

Chemicals: all chemical used Cu (II), Pb(II), Mn(II), Co(II) nitrate were used and obtained as AnalR (Obtained from Fluke) and these metal ions were standardized against Na₂EDTA. Distal deionized water was used for all preparations. Hydrochloric acid and sodium hydroxide were all pure solution (Obtained from Fluke)

Instrumentations:

All the following instruments were calibrated by using standard solutions or reference material to obtain the satisfaction:

- 1- Atomic absorption spectrophotometer used was Shimadzu AA-6200.
- 2- FT-IR spectrophotometer – Shimadzu.
- 3- pH meter was Research pH meter Radiometer, Copenhagen, Denmark.
- 4- Shaker was BS-11 digital, JEIO TECH, Korea.

Procedures:

1-Preparation of adsorbent; MC leaves were collected from gardens of Al-Mustansyria University, Baghdad, Iraq. The leaves were extensively washed with deionized water to remove dirt, dried in an oven at 80°C for a period of 3hr, then ground and screened to obtain the average particle size (300, 500, 700 μm). The powder was preserved in glass bottles for use as adsorbent.

2-Preparation of spiked wastewater; Prepare series of diluted Cu (II), Pb(II), Mn(II) and Co(II) solutions (10-50 mg/L) from stock solution (each metal ion was prepared separately). All measurements of metal ions

before and after adsorption were measured by atomic absorption spectrophotometric (shemadzu AA 6200).

3-Batch adsorption procedures; to measure the adsorption of metal ions on MC different weights of adsorbents were used at concentration of 10-50 mg/L. all parameters (pH, contact time, weight of adsorbent, temperature, initial concentration and particle size) were kept constant except one which was variable. Measure concentration of metal ions before and after adsorption by flame atomic absorption.

4-calculation of adsorption efficiency and distribution coefficient (kd).

The adsorption capacity may be calculated by the flowing equation;

$$Q_e = v (c_o - c_e) / m \dots 1 \quad (14)$$

Q_e =adsorption capacity , v = suspension volume , m = mass of adsorbent material (g), c_o =initial concentration , c_e =final concentration.

k_d can be defined as a measure of the efficiency of binding for bounded to the surface of adsorbent. The k_d may be calculated by the flowing equation;

$$K_d = r_{ws} (C_o - C_e) / C_e \dots 2$$

r_{ws} ;the ratio between the volume of the adsorbent solution to the weight of adsorbent(ml/g), C_o and C_e are primary and final concentration of adsorbed material, respectively (mg / L).

5-FT-IR Characterization of MC:FTIR apparatus type shimadzu (4000-400 cm^{-1}) was carried out in order to identify the functional groups in the MC leaf powder that might be involved in the adsorption process.

Results and discussion:

FTIR characterization: The Characterization of MC powdered was given in fig 1. In this fig the following peaks were 3419.56, 2929.67 and 1739.67 cm^{-1} which were assigned to alcoholic O-H, stretching, CH₂ and ketonic C=O respectively [15]. It is clear from this characterization that the mc adsorbent has the activity to bind with the action by the function group which contains one pairs of electrons which explain the capacity of this adsorbent.

Optimization results:

Effect of pH; The pH is considered one of the most important parameters of biosorption of heavy metals [16]. However the adsorption of these heavy metals Cu(II), Pb(II), Mn(II), and Co(II) on by mc powder were found different at pH values 2-6 and results were given in Fig 2. From this Fig, the order of pH adsorption was 6, 4, 3 and 4 respectively. Using 2.0g of the adsorbent with 50ml of Cu(II), Pb(II), Mn(II), Co(II) ions solution, the percentage of adsorption were 89.52%, 97.24%, 82.72%, 70.8% respectively. At pH higher than 6 both metals were

precipitated due to the formation of hydroxides and removal due to sorption was very low. The minimal adsorption at low pH may be due to the higher concentration and high mobility of the H⁺, which are preferentially adsorbed rather than the metal ions [17, 18]. At higher pH values, the lower number of H⁺ and greater number of ligands with negative charges results in greater Cu(II), Pb(II), Mn(II), Co(II) adsorption. For example, carboxylic groups (-COOH) are important groups for metal uptake by biological materials [19, 20]. At pH higher than 3-4, carboxylic groups are deprotonated and negatively charged. Consequently, the attraction of positively charged metal ions would be enhanced [21]. In summary, the order of adsorption efficiency as follows; Pb(II) > Cu(II) > Mn(II) > Co(II).

Effect of adsorbent weight: To obtain the highest percentage removal of heavy metals different amounts (0.5-3g) of adsorbent were examined at optimum conditions. Results are given in fig 3. The removal percentages of Cu(II), Pb(II), Mn(II), Co(II) ion on MC powder were Pb(II) 98.8%, > Cu(II) 92.4%, > Mn(II) 84.37%, > Co(II) 72.2%. The difference in adsorption capacity of these metal ions may be explained due to the greater availability of the exchangeable sites or surface area at higher concentration of the adsorbent [22].

Effect of Initial Concentration of Cu(II), Pb(II), Mn(II), Co(II) ions: In order to achieve maximum adsorption the initial concentration of metal ion should be optimum at fixed conditions. Therefore different concentration of metal ions (10-50 mg/l). Following general procedure given previously (procedure 2), results are given in fig 4. From the results the sequence of adsorption was found; Pb(II) (98.8%) > Cu(II) (92.4%) > (Mn(II) (84.37%) > Co(II) (72.2%) and these results are achieved at initial concentration (10-50 mg/l). Such results may be due to the adsorption of heavy metals by specific sites provided by the acidic functional groups on the biocarbon, while with increasing metal concentrations the specific sites are saturated and the exchange sites due to excessive surface area of the biocarbon are filled [23].

Effect of contact time: This parameter is important as it is affecting the removal percentage of metal ions, therefore effect of contact time was studied by fixing all parameter expect time which was varied to 90 min. results are given at Fig 5 which shows that maximum removal was attained at 90 min. The comparison of the four ions were found; Pb(II) 94.4% > Cu(II) 89.6% > (Mn(II) 84.16% > Co(II) 69.6%. The rate of metal removal was found higher at beginning due to a larger surface area of the adsorbent being available for the adsorption of the metal [24]. Equilibrium time was found to be different in each metal ions due to physical and chemical properties of each metal.

Effect of Temperature: Temperature is another parameter has been studied to obtain maximum removal of heavy metals. By fixing all parameters expect temperature was varied from 25 to 70°C. Results are given in fig 6. results show that the removal percentage of heavy metals was found: Pb(II)(97.16%)>Cu(II)(92.08%) > (Mn(II)(83.14%)>Co(II)(79.72%). It is obvious that optimum temperature is 25°C for Co(II),Mn(II) metal ions and 60,70 °C for Cu(II),Pb(II) metal ions respectively . The interactions were found to be exothermic and endothermic in nature [25-26] the Pattern of the process is endothermic for Cu(II),Pb(II) metal ions; therefore increase in uptake of metal ions was increased with temperature while the Pattern of the process is exothermic for Co(II),Mn(II) metal ions .

Adsorption models

Langmuir, Freundlich and Temkin models are commonly used to follow experimental data [28-29].

The final results of adsorption were found to fit Freundlich isotherm model better than Langmuir and Temkin isotherm. To compare the adsorption model of metals, figures 7-10 show that the regression coefficient (R²) were found (0.999,0.990,0.996 and 0.997) for Cu(II),Pb(II),Mn(II) , and Co(II) ions respectively.

The Freundlich isotherm is described by equation below;

$$\text{Log}q_e = \text{log} K_F + 1/n \text{ log} C_e$$

Where q_e is the amount of adsorbate, C_e is the equilibrium concentration of metal ion, while n and K_F are empirical Freundlich constants. n was found from slop of the curve . K_F was calculated from the intercept. The values of these constants, listed in table (1). K_d value for lead ions was higher than other metals ions (1.59) .the squance of capacity of metal ions were founded to be in the order; Pb>Cu>Mn>Co.

Adsorption Kinetics:

Fig. 11 shows the behavior of adsorption (II), Pb(II),Mn(II), and (II) ions on MC leaf powder at optimum conditions . All curves proved that adsorption was linear and pseudo-second order equation [31 - 32]. The sequence of adsorption are Mn>Pb>Co>Cu. This difference in adsorption can be used for separation of these metal ions using other technique.

Distribution coefficient (kd)

By applying the equation 2 to calculate k_d values in table 2 explained that k_d values of copper is low (278.94-644.44), for cobalt , k_d values are smaller (26.25-30.45); for manganese k_d values were also low (111.6-181.61) . Therefor adsorption efficiency for Co and Mn are weak but for Cu is higher than Co and Mn ions. Only lead ions have higher k_d .

Therefore this adsorbent (mc) can be used for separation of lead in the presence metals ions. Although k_d values for Cu, Co and Mn are low but Mc still useful for removal of heavy metals.

Conclusion;

MC was proved successful for removal of Cu (II), Pb(II),Mn(II), and Co (II) ions from waste water (72.2-98.8%). The Freundlich isotherm model was better used to represent the experimental data. From the results different k_d values are shown and the selectivity was founds in the following sequence; Pb> Cu>Mn>Co, therefore separation can be achieved using other technique such as ion exchange chromatography. K_d values were found less than 1000 for Cu, Mn and Co but higher than 1000 for Pb ions.

References;

- (1) Al-Garni SM; Biosorption of lead by Gram-ve capsulated and non-capsulated bacteria, Water SA 31,345–50,(2005)
- (2) O.J. Esalah, M.E. Weber and J.H. Vera, Removal of lead, cadmium and zinc from aqueous solutions by precipitation with sodium di-(*n*-octyl) phosphinate Can. J. Chem. Eng., 78, 948–954(2000).
- (3) A.I. Zouboulis, K.A. Matis, B.G. Lanara and C.L. Neskovic, Removal of cadmium from dilute solutions by hydroxy apatite. II. Floatation studies, Sep. Sci. Technol., 32, 1755–1767,(1997).
- (4) Y.S. Ho, J.C.Y. Ng and G. McKay, Removal of lead (II) from effluents by sorption on peat using second-order kinetics, Sep. Sci. Technol., 36, 241–261(2001).
- (5) C. Hall, D.S. Wales and M.A. Keane, Copper removal from aqueous systems: biosorption by pseudomonas syringae, Sep. Sci. Technol., 36,223–240(2001).
- (6) Y. Sag, B. Akcael and T. Kutsal, Ternary biosorption equilibria of chromium (VI), copper (II) and cadmium(II) on Rhizopus Arrhizus, Sep. Sci. Technol., 37, 279–309(2002).
- (7) L. Canet, M. Ilpide and P. Seat, Efficient facilitated transport of lead, cadmium, zinc and silver across a flat sheet-supported liquid membrane mediated by lasalocid A, Sep. Sci. Technol., 37, 1851–1860(2002).
- (8) sunil k. bajpai, arti j. ; removal of copper(ii) from aqueous solutions using spent tea leaves (STL) as a potential sorbent , Water SA (on line) vol.36(3) (2010).
- (9) Hengpeng Ye, Linzhang , beeping zhang, guominwu; adsorption removal of cu(II) from aqueous solution using modified rice husk, IJERA, vol.2(2), 855–863(2012).
- (10) V. Ravindran, M.R. Stevens, B.N. Badriyha and M. Pirbazari, Modeling the sorption of

- toxic metalsonchelant-impregnated adsorbent, *AICHE J.*, 45,1135–1146(1999).
- (11) C.A. Toles and W.E. Marshall, Copper ion removal by almond shell carbons and commercial carbons:batch and column studies, *Sep. Sci. Technol.*, 37,2369–2383(2002).
- (12) G.H. Pino, L.M.S. de Mesquita, M.L. Torem and G.A.S. Pinto, Biosorption of cadmium by green coconut shell powder, *Miner. Engin.*,(2006).
- (13) K.N. Ghimire, K. Inoue, H. Yamaguchi, K. Makino, T. Miyajima, Adsorptive separation of arsenate and arsenite anions from aqueous medium by using orange waste, *Water Res.* 37 4945–4953(2003).
- (14) S.E.Elaigwu, L.AUsman, G.V.Awolola, G.B.Adebayo, R.M.K.Ajayi; Adsorption of Pb(II) fromAqueous solution by Activated Carbon prepared from Cow Dung :Adv .in.Appl.Sci.,3(3):442-446(2009).
- (15) Pretsch ,E.,Clem ,T.,Seihl,J.,andSimon,W;SpectraData for Structure Determination of organic Compounds.Berlin:Springer-Verlag.(1981).
- (16) Aksu Z; Equilibrium and kinetic modelling of cadmium (II) biosorption by *C. vulgaris* in a batch system: effect of temperature. *SeparPurif Tech* 21,285–294.
- (17) S.H. Lee, C.H. Jung, H. Chung, M.Y. Lee, J.-W. Yang, Removal of heavy metals from aqueous solution by apple residues, *Process.Biochem.*33 ,205–211(1998).
- (18) G. Annadurai, R.-S.Juang, D.-J. Lee, Use of cellulose-based wastes for adsorption of dyes from aqueous solutions, *J. Hazard. Mater.* 92 (3),263–274(2002).
- (19) F. Pagnanelli, M.P. Petrangeli, L. Toro, M. Trifoni, F.Veglio, Biosorption of metal ions on *Arthrobactersp.*: biomass characterization and biosorption modeling, *Environ.Sci.Technol.* 34, 2773–2778(2000).
- (20) M. Ajmal, R.A.K. Rao, R. Ahmad, J. Ahmad, Adsorption studies on *Citrus reticulata*: removal and recovery of Ni (II) from electroplating wastewater,*J. Hazard. Mater.* B79,117–131(2000).
- (21) L. Norton, K. Baskaran, T. McKenzie, Biosorption of zinc from aqueous solutions using biosolids, *Adv. Environ. Res.* 8,629–635(2004).
- [39] D. Kratochvil, B. Volesky, Advances in the biosorption of heavy metals, *Trends Biotechnol.* 16,291–300(1998).
- (22) S.H. Lee, C.H. Jung, H. Chung, M.Y. Lee, J.-W. Yang,;Removal of heavy metals from aqueous solution by apple residues, *Process. Biochem.*33,205–211(1998).
- (23) El-Ashtoukhy ESZ, Amina NK, AbdelwahabO;Removal of lead (II) and copper (II) from aqueous solution using pomegranate peel as a new adsorbent. *Desalination* 223, 162–73(2008).
- (24) Yu,Q.andKaewsarn, p.;Biosorption of copper(II) from aqueous solution by pre-treated biomass of marine alga *padina sp.**Chemosphere.*47,1081-1085(2002).
- (25) SharmaA and Bhattacharyya KG, *Azadirachta indica* (Neem) leaf powder as a biosorbent for removal of Cd (II) from aqueous medium. *J. Hazard.Mater.* B125, 102 – 112(2005).
- (26) Khormaei M, Nasernejad B, Edrisi M and Eslamzadeh T, Copper biosorption from aqueous solution by sour orange residue. *J.Hazard.Mater.* 149, 269 – 274 (2007).
- (27) Prasanna Kumar Y, King P, Prasad VSRK, Equilibrium and kinetic studies for the biosorption of copper (II) ion from aqueous solution using *TectonagrandisL.f* leaves powder. *J. Hazard. Mater.* B137: 1211 – 1217 (2006).
- (28) Stephen, I.B. and Sulochana, N.;Carbonised Jackfruit peel as an adsorbent for the Removal of Cd(II) from Aqueous Solution. *Biores Technol.* 94:49-52 2004.
- (29) Bunluesin, S., Kruatrachue, M. and Pokethitiyook,P.. Batch and continuous packedcolumnstudiesofcadmiumbiosorption byHydrillaverticillatabiomass.*BiosciBioeng.* 103,509-513(2007).
- (30) Temkin,M.J.and V.Pyzhev,.*Acta.Physioshim.URSS.*,12:217-222(1940).
- (31) J. Yu, M.Tong, X. Sun and B. Li, “Cystin-modified for Cd (II) and Pb(II) biosorption,” *Hazardous Materials.*, 143, pp. 277-284, (2007).
- (32) B. Benguella and H. Benaissa, “Cadmium removal from aqueous solution by chitin: kinetic and equilibrium studies,” *Water Resource.*,vol. 36, pp. 2463–2474(2002).

Table (1) Freundlich parameter for the adsorption of heavy metals on myrtus communis leaves powder

Absorbate	Parameters		R ²
Cu	N	1.57	0.999
	K _f	0.57	
Co	N	1.1	0.997
	K _f	0.035	
Pb	N	1.59	0.991
	K _f	1.01	
Mn	N	1.34	0.996
	K _f	0.2	

Table (2); Distribution coefficient of Cu,Co,Pb and Mn ions on MCl leaf powder at 25°C under optimum condition.

Ions	Co mg/l	Ce mg/l	r ws	Kd
Cu	10	0.72	50	644.44
	20	2.08		430.76
	30	3.72		353.22
	40	5.6		307.14
	50	7.6		278.94
Co	10	3.964	20	30.45
	20	8		30
	30	12.01		29.95
	40	17.05		26.92
	50	21.62		26.25
Pb	10	0.12	25	2058.33
	20	0.28		1760.71
	30	0.59		1246.18
	40	0.94		1038.82

	50	1.4		867.85
Mn	10	1.21	25	181.61
	20	2.7		160.18
	30	4.58		138.75
	40	6.98		118.26
	50	9.16		111.46

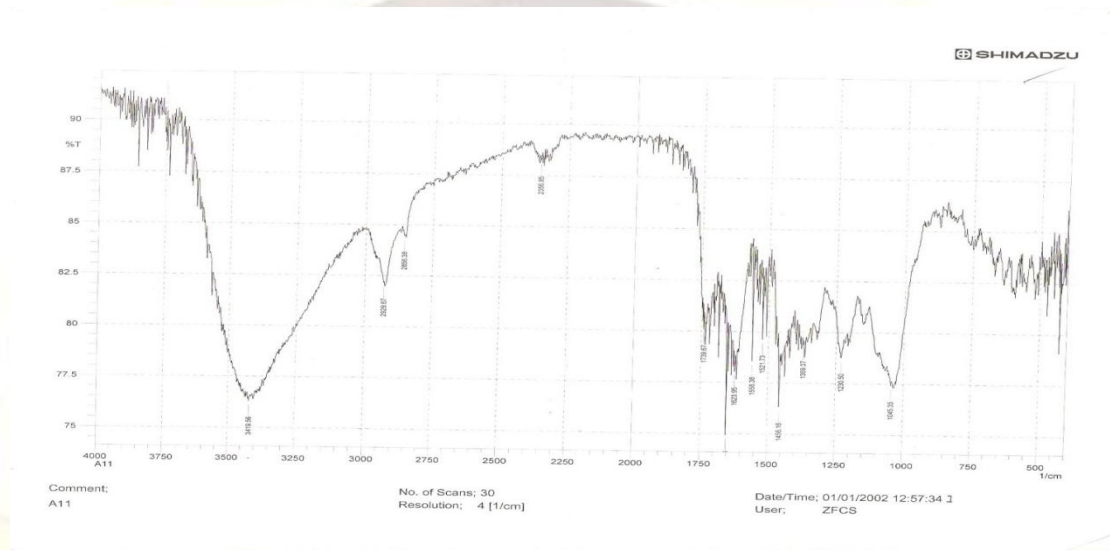


Fig (1) FTIR of MC leaf powder

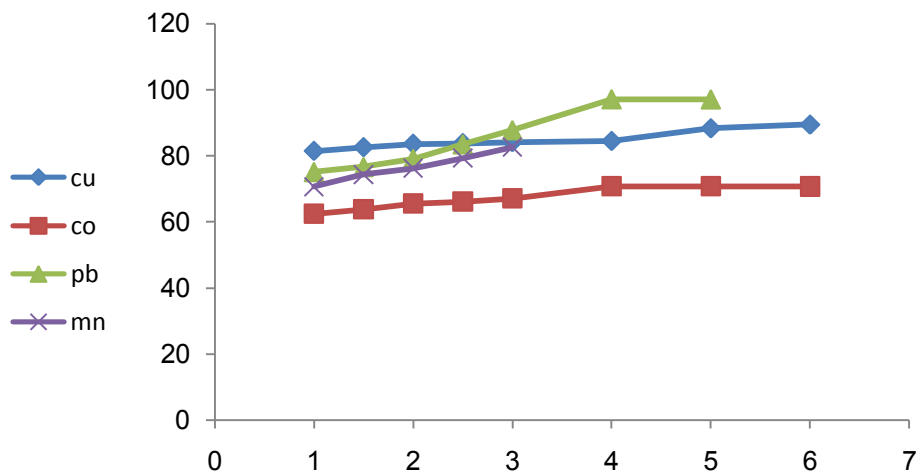


Fig (2) Effect of pH on adsorption of Cu, Co, Pb and Mn

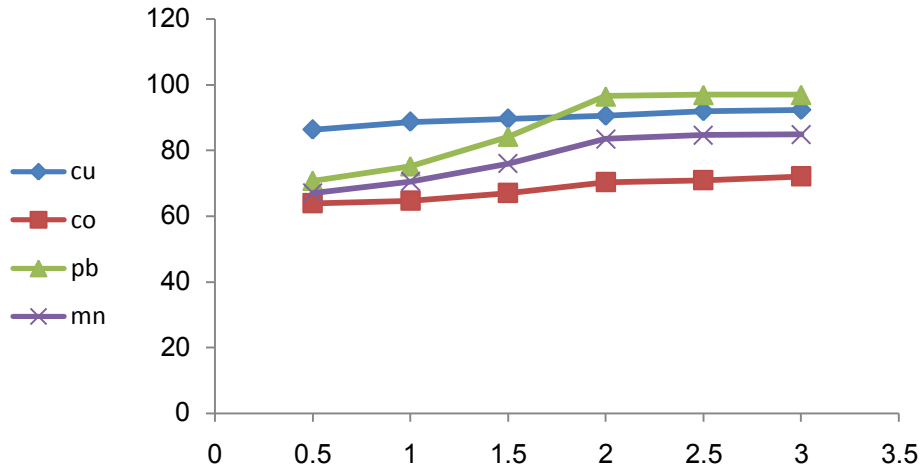


Fig (3) Effect of adsorbent weight on adsorption of Cu, Co, Pb and Mn

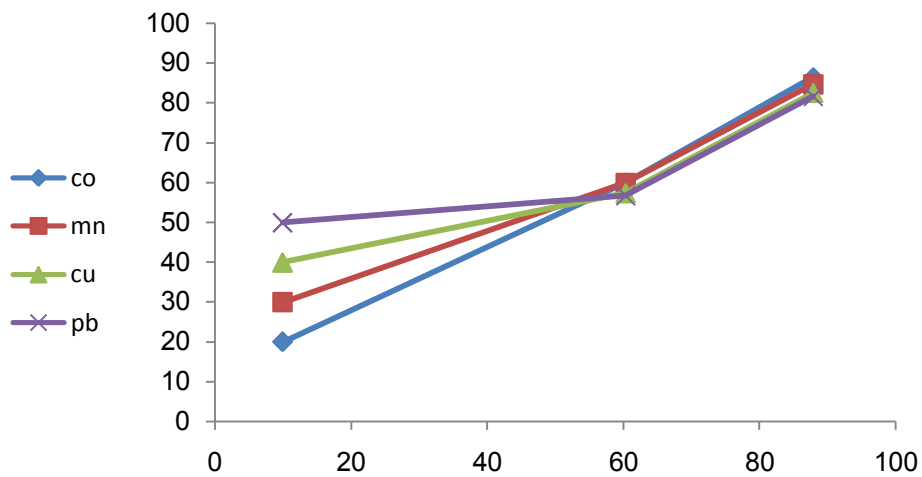


Fig (4) Effect of concentration on adsorption of Cu, Co, Pb and Mn

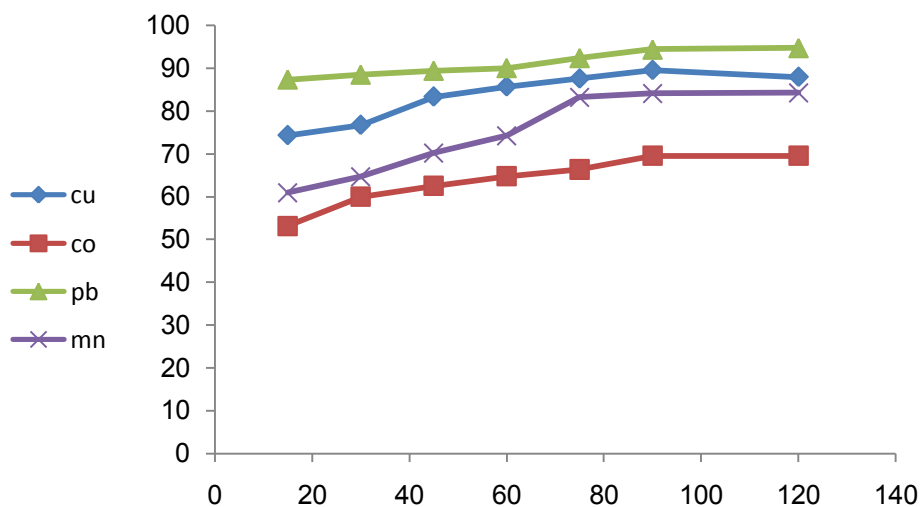


Fig (5) Effect of contact time on adsorption of Cu, Co, Pb and Mn

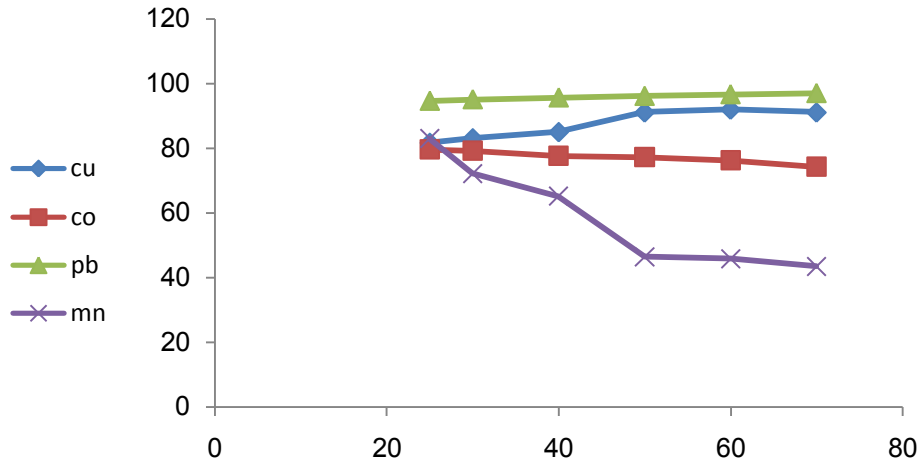


Fig (6) effect of temperature on adsorption of Cu,Co,Pb and Mn

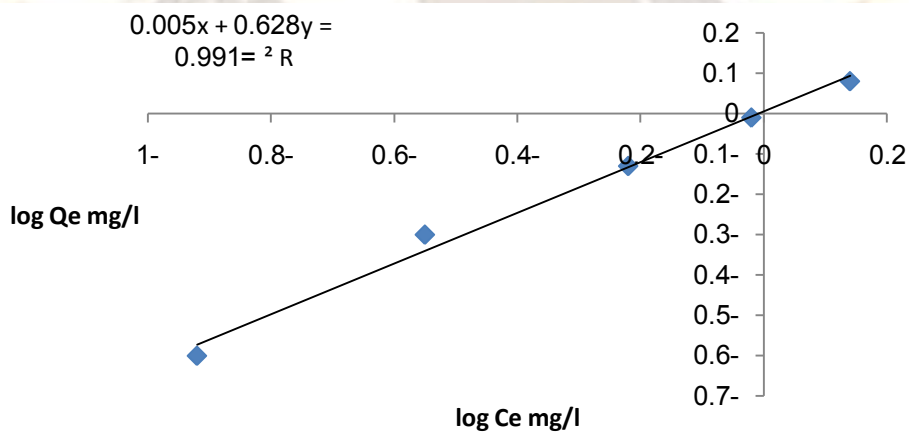


Fig (7) Freundlich isotherm for the adsorption of Pb (II) ion on MC leaf powder at 25°C under optimum conditions

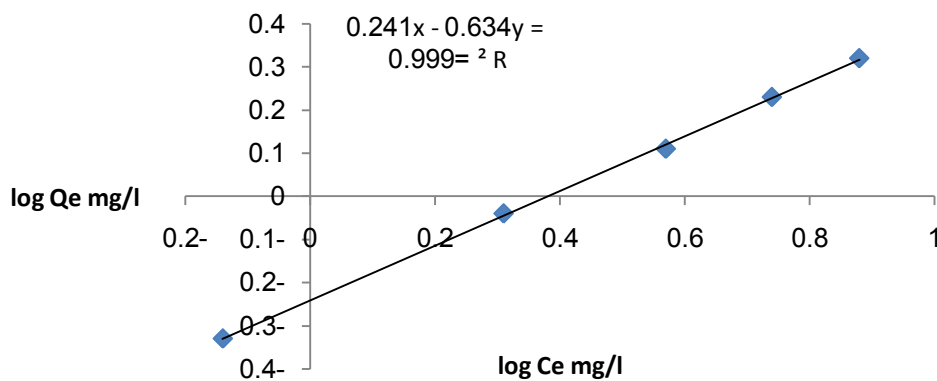
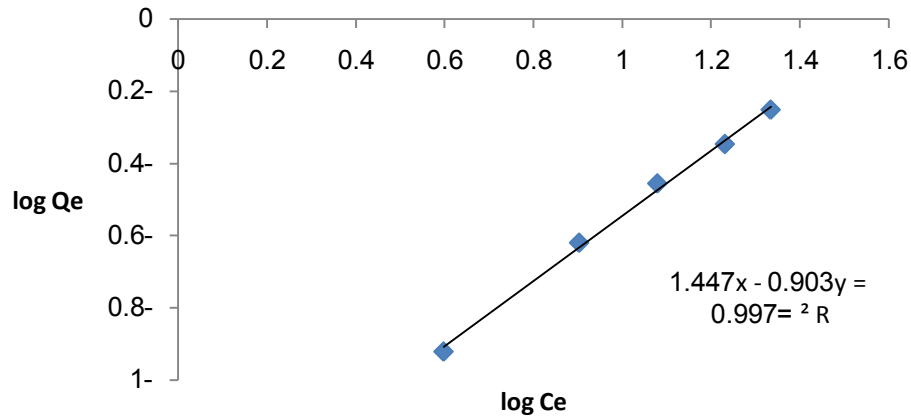


Fig (8) Freundlich isotherm for the adsorption of Cu (II) ion on MC leaf powder at 25°C under optimum conditions



Fig(9) Freundlich isotherm for the adsorption of Co (II) ion on Mc powder at 25°C under optimum conditions

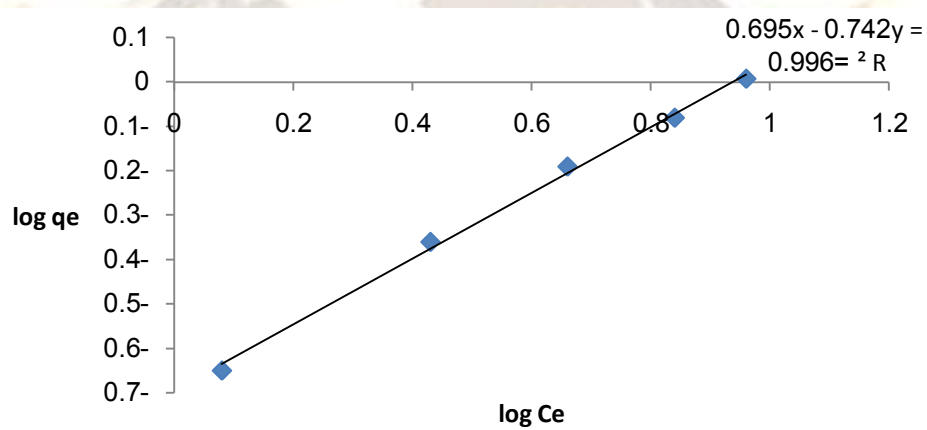


Fig (10) Freundlich isotherm for the adsorption of Mn (II) ion on MC leaf powder at 25°C under optimum conditions

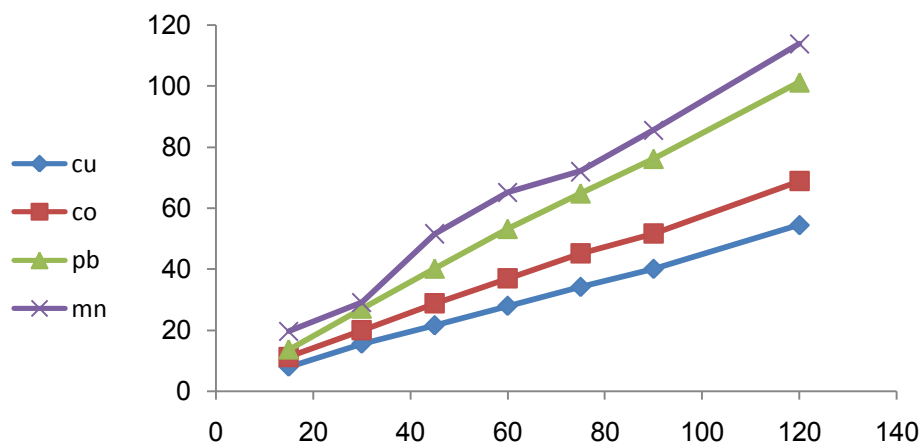


Fig (11) second order for the adsorption of Cu (II), CO (II), Pb(II), Mn(II) ions on MC leaf powder at 25°C under optimum conditions